

# Exploring the dynamic evolution of lattice oxygen on exsolved-Mn<sub>2</sub>O<sub>3</sub>@SmMn<sub>2</sub>O<sub>5</sub> interfaces for NO Oxidation

Received: 15 November 2023

Accepted: 8 August 2024

Published online: 02 September 2024

Check for updates

Xiyang Wang<sup>1,2,7</sup>, Qilei Yang<sup>1,7</sup>, Xinbo Li<sup>3</sup>, Zhen Li<sup>1</sup>, Chuan Gao<sup>1</sup>, Hui Zhang<sup>4</sup>, Xuefeng Chu<sup>1</sup>, Carl Redshaw<sup>5</sup>, Shucheng Shi<sup>6</sup>, Yimin A. Wu<sup>2</sup>, Yongliang Ma<sup>1</sup>, Yue Peng<sup>1</sup>✉, Junhua Li<sup>1</sup> & Shouhua Feng<sup>3</sup>

Lattice oxygen in metal oxides plays an important role in the reaction of diesel oxidation catalysts, but the atomic-level understanding of structural evolution during the catalytic process remains elusive. Here, we develop a Mn<sub>2</sub>O<sub>3</sub>/SmMn<sub>2</sub>O<sub>5</sub> catalyst using a non-stoichiometric exsolution method to explore the roles of lattice oxygen in NO oxidation. The enhanced covalency of Mn–O bond and increased electron density at Mn<sup>3+</sup> sites, induced by the interface between exsolved Mn<sub>2</sub>O<sub>3</sub> and mullite, lead to the formation of highly active lattice oxygen adjacent to Mn<sup>3+</sup> sites. Near-ambient pressure X-ray photoelectron and absorption spectroscopies show that the activated lattice oxygen enables reversible changes in Mn valence states and Mn–O bond covalency during redox cycles, reducing energy barriers for NO oxidation and promoting NO<sub>2</sub> desorption via the cooperative Mars-van Krevelen mechanism. Therefore, the Mn<sub>2</sub>O<sub>3</sub>/SmMn<sub>2</sub>O<sub>5</sub> exhibits higher NO oxidation activity and better resistance to hydrothermal aging compared to a commercial Pt/Al<sub>2</sub>O<sub>3</sub> catalyst.

Considering the high fuel efficiencies, diesel engines are prominently utilized in heavy-duty vehicles, construction equipment and industrial machinery etc<sup>1,2</sup>. The diesel oxidation catalyst (DOC), integral in these applications, is used to oxidize CO and hydrocarbons to CO<sub>2</sub>, as well as also converting emitted NO to NO<sub>2</sub> during NO oxidation<sup>2–4</sup>. Where the produced NO<sub>2</sub>, possessing higher oxidation ability than O<sub>2</sub>, is used to oxidize the soot in the back-end diesel particulate filters at low temperatures, making it a key performance indicator of DOCs<sup>5,6</sup>. Conventionally, Pt-based catalysts are used as commercial DOCs, yet they face substantial drawbacks including cost and sintering issues<sup>6–9</sup>. Hence, the thrust towards Pt-free catalysts with good thermal stability such as mullites (AB<sub>2</sub>O<sub>5</sub>) is gaining much attention as one of the next-generation DOCs to meet the increasingly stringent regulations in the US, EU etc<sup>10–13</sup>. Despite the significant progress achieved in NO

oxidation on metal-oxide catalysts, the dynamic evolution mechanism of mullite catalysts remains enigmatic.

Over the past few decades, it has been generally believed that NO oxidation on metal oxides is catalyzed solely by surface cations, following the Eley-Rideal (E-R) mechanism. To enhance the catalytic performance, traditional improvement strategies focused on the secondary metal doping modifications in the valence state of the surface metal sites<sup>14,15</sup> and in decomposition of nitrate or nitrite species on catalysts<sup>16,17</sup>. Wang et al.<sup>2</sup> demonstrated that a Sr-doped mullite exhibits even higher activity for NO oxidation compared to a commercial Pt/Al<sub>2</sub>O<sub>3</sub> (87% versus 55% NO conversion at 300 °C). The good activity was attributed to an increased formation of nitrates at surface-exposed Mn<sup>4+</sup> sites, which allowed for facile decomposition to NO<sub>2</sub>. However, recent results challenged the notion that metal or surface cation sites

<sup>1</sup>School of Environment, Tsinghua University, Beijing, PR China. <sup>2</sup>Department of Mechanical and Mechatronics Engineering, Waterloo Institute for Nanotechnology, Materials Interface Foundry, University of Waterloo, Waterloo, ON, Canada. <sup>3</sup>State Key Laboratory of Inorganic Synthesis and Preparative Chemistry, College of Chemistry, Jilin University, Changchun, PR China. <sup>4</sup>State Key Laboratory of Functional Materials for Informatics, Shanghai Institute of Microsystem and Information Technology, Chinese Academy of Sciences, Shanghai, PR China. <sup>5</sup>Chemistry, School of Natural Sciences, University of Hull, Hull, UK. <sup>6</sup>School of Physical Science and Technology, Shanghai Tech University, Shanghai, PR China. <sup>7</sup>These authors contributed equally: Xiyang Wang, Qilei Yang. ✉e-mail: pengyue83@tsinghua.edu.cn

alone are responsible for catalytic activity<sup>3,8,18</sup>. It has been found that surface lattice oxygen ( $O_{\text{latt}}$ ) of metal oxides can directly participate in some redox reactions. For instance, surface oxygen exchange kinetics in solid oxide fuel cells<sup>19,20</sup>, oxygen evolution in water splitting<sup>21–23</sup>, and lithium storage capacity in batteries<sup>24–26</sup>. In addition, the introduction of oxygen vacancies<sup>27–29</sup> or the doping of isovalent A/B-site cations in metal oxides<sup>29–31</sup> can also enhance the oxidation ability with/without varying the valence state of metal sites. Our previous work also indirectly pointed out that removing inactive Sm ions of a mullite catalyst surface could enhance the covalency of the Mn–O bond, improve the lattice oxygen activity, and exposed more  $Mn^{4+}$  ions to facilitate the decomposition of nitrate species<sup>16,17</sup>, but the detailed roles and mechanism of lattice oxygen during NO oxidation remained elusive due to the interference of  $Mn^{4+}$  ions and the E-R mechanism. Recent density functional theory (DFT) calculations suggested that surface lattice oxygen on metal oxides may serve as exceptionally active sites in NO oxidation, with lower energy barriers in NO oxidation compared to traditional metal sites<sup>10,32–34</sup>. Zheng et al. theoretically unraveled the cooperative Mars-van Krevelen (MvK) mechanism on the  $O_{\text{latt}}$  sites around  $Mn^{3+}$  ions and the nitrite intermediates<sup>10</sup>, enhancing the understanding of  $O_{\text{latt}}$  sites in metal oxide catalysts during NO oxidation. However, the dynamic structure evolutions of cations and  $O_{\text{latt}}$  sites during real-time reactions are poorly understood because of the limited direct experimental evidence in monitoring the reaction process<sup>35</sup>. The methodology of in-situ technologies is essential to address this knowledge gap and promote the clarification of chemical descriptors (for example, valence state, bond covalency, electron density, etc.) and reaction mechanisms at the atomic level.

In this study, we provide insights into the underlying active sites of traditional mullite  $SmMn_2O_5$  (SMO) and  $Mn_2O_3/SmMn_2O_5$  ( $Mn_2O_3$ /SMO) catalysts with exsolved- $Mn_2O_3$  on the SMO surface via the nonstoichiometric exsolution method. Leveraging an array of near ambient pressure X-ray photoelectron/absorption spectroscopies (NAP-XPS and NAP-XAS), we directly observed that the NO oxidation process on  $Mn_2O_3$ /SMO relies on the dynamic covalency variations of the Mn–O bond at  $O_{\text{latt}}$  adjacent to the  $Mn^{3+}$  cations. Unlike the E-R mechanism occurring at  $Mn^{4+}$  sites, the  $O_{\text{latt}}$  of  $Mn_2O_3$ /SMO predominantly follows the cooperative MvK mechanism, and the induced  $O_{\text{latt}}$ -NO<sub>2</sub> nitrite species facilitates the NO<sub>2</sub> desorption. This work identifies the  $O_{\text{latt}}$  as the active site both theoretically and experimentally, and further sheds light on the mechanism of NO oxidation.

## Results

### Structure of the catalyst interface

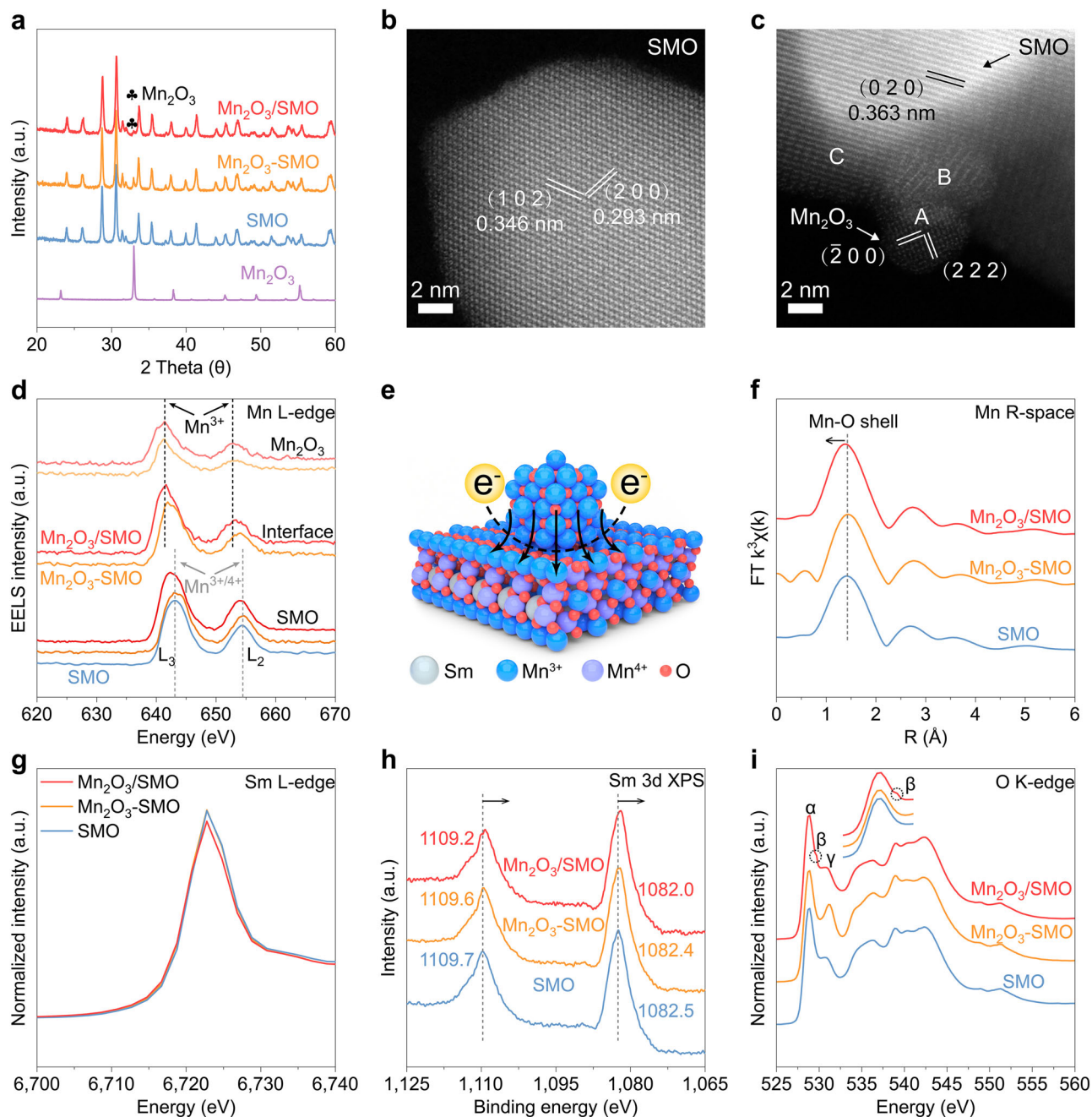
The  $Mn_2O_3$ /SMO catalyst was prepared by the nonstoichiometric exsolution method. During a high-temperature calcination (800 °C), a surplus of  $MnO_x$  was accumulated on the mullite (SMO) surface and transitioned into a stable  $Mn_2O_3$  phase. Pristine SMO,  $Mn_2O_3$ , and the co-impregnated sample of  $Mn_2O_3$  on SMO ( $Mn_2O_3$ -SMO) were synthesized and calcined at 800 °C<sup>16,17</sup>. The X-ray diffraction (XRD) results depicted confirm that the  $Mn_2O_3$ /SMO possesses a mullite structure whilst further containing an exsolved- $Mn_2O_3$  phase at 32.9° (Fig. 1a). The main diffraction peak (211) of  $Mn_2O_3$ /SMO exhibits an obvious shift compared to that of SMO and  $Mn_2O_3$ -SMO (Supplementary Fig. 1), suggesting the lattice contraction occurs on the mullite support of  $Mn_2O_3$ /SMO. The refined XRD results of SMO and  $Mn_2O_3$ /SMO (Supplementary Fig. 2 and Supplementary Table 1) also demonstrate that the lattice constant and unit cell volume parameter of SMO change from  $a = 7.44$  Å ( $V = 363.53$  Å<sup>3</sup>) to  $a = 7.43$  Å of  $Mn_2O_3$ /SMO ( $V = 362.6$  Å<sup>3</sup>). Such a lattice contraction is mainly attributed to the produced oxygen vacancies and interface interactions.

The interface atomic structure was imaged utilizing high-angle annular dark field scanning transmission electron microscopy (HAADF-STEM), revealing that the spacings of the lattice fringe on the SMO sample are 3.46 and 2.93 Å, assignable to the (102) and (200)

facets of mullite, respectively (Fig. 1b and Supplementary Figs. 3–4). It is interesting to note that the spacing on the  $Mn_2O_3$ /SMO is 3.63 Å, assignable to the (020) facet of mullite (Fig. 1b, c), coherently aligning with the peak shift in the XRD results. The spacings of the lattice fringe on the exsolved oxide region can be allocated to the (200) and (222) facets of the  $Mn_2O_3$  phase. The electron energy loss spectroscopy (EELS) reveals intricate details about the local electronic structure of catalysts. Mn L-edge EELS spectra (Fig. 1d) show that the  $Mn_2O_3$ /SMO contains more  $Mn^{3+}$  cations and lower shifts for peak positions than does  $Mn_2O_3$ -SMO at the interface and mullite regions, but a single SMO surface exists with the same Mn valence states and peak positions with mullite regions of  $Mn_2O_3$ -SMO. These results directly imply that the exsolved  $Mn_2O_3$ /SMO possesses strong interface interactions while there is a negligible interfacial interaction on  $Mn_2O_3$ -SMO. The Mn L-edge EELS results highlight that the conventional impregnation method can only present a slight impact on the electronic structure between  $Mn_2O_3$  and SMO. However, the interface between exsolved- $Mn_2O_3$  and SMO of  $Mn_2O_3$ /SMO presents an important electron enrichment on Mn atoms, which is a prerequisite for generating a robust electron transfer at the interface. Furthermore, O K-edge EELS spectra reveal that the Mn–O bond covalency at the SMO surface of exsolved  $Mn_2O_3$ /SMO is stronger than mullite and the deposited  $Mn_2O_3$ -SMO due to the higher energy position for the adsorption peak of the Mn–O bond (Supplementary Fig. 5). While both SMO and  $Mn_2O_3$ -SMO show the same covalency of Mn–O bond because of the same peak position. These results demonstrate the interface interactions and the activation of lattice oxygen in exsolved  $Mn_2O_3$ /SMO. A schematic representation of the electron transfer at the interface (Fig. 1e) reveals that the electron transfer from exsolved  $Mn_2O_3$  to SMO activates the  $O_{\text{latt}}$  sites of  $Mn_2O_3$ /SMO.

The H<sub>2</sub> temperature programmed reduction (H<sub>2</sub>-TPR) profiles (Supplementary Fig. 6) infer that the  $Mn^{4+}$  of  $Mn_2O_3$ /SMO exhibits a slightly lower reduction peak at 410 °C than the other samples, suggesting its high reducibility. The O<sub>2</sub> temperature programmed desorption (O<sub>2</sub>-TPD) profiles (Supplementary Fig. 7) manifest that  $Mn_2O_3$ /SMO possesses more adsorbed oxygen species below 180 °C and the considerable amount of active surface  $O_{\text{latt}}$  occurring at 180–300 °C. The NO temperature programmed desorption (NO-TPD) profiles (Supplementary Fig. 8) display a lower temperature for NO<sub>x</sub> desorption at 150 °C on  $Mn_2O_3$ /SMO. The above results confirm that the interface between exsolved- $Mn_2O_3$  and the mullite support of  $Mn_2O_3$ /SMO can improve the reducibility of surface Mn and the number of  $O_{\text{latt}}$ , enhancing the NO<sub>x</sub> desorption ability at low temperatures.

Mn K-edge X-ray absorption near edge structure (XANES) and extended X-ray absorption fine (EXAFS) spectroscopies reveal that the  $Mn_2O_3$ /SMO possesses the same average valence state of bulk Mn atoms with  $Mn_2O_3$ -SMO due to the similar adsorbed edge position and exhibits a shorter Mn–O bond length compared to  $Mn_2O_3$ -SMO and SMO (Fig. 1f and Supplementary Figs. 9, 10). This result demonstrates the important effect of the exsolved interface on tuning the Mn coordination environment and surface electronic state because the average valence of the bulk Mn atom has little relevance with the interface. Furthermore, the Sm L<sub>3</sub>-edge XANES spectra (Fig. 1g) demonstrate that  $Mn_2O_3$ /SMO possesses a weaker intensity of white line peak than  $Mn_2O_3$ -SMO and SMO, resulting in an increased number of electrons at the Sm sites. The consequential electron transfer and ensuing modifications are further confirmed by a shift in the Sm 3d spectra of X-ray photoelectron spectroscopy (XPS) (Fig. 1h). With respect to the Mn L-edge XAS spectra (Supplementary Fig. 11),  $Mn_2O_3$ /SMO presents a lower intensity of white line peak and a diminished peak intensity ratio of L<sub>3</sub>/L<sub>2</sub> compared to SMO and  $Mn_2O_3$ -SMO, suggesting that the  $Mn_2O_3$ /SMO hosts surplus electrons in the Mn 3d orbitals. An exploration of O K-edge XAS spectra on  $Mn_2O_3$ /SMO indicates notable variations in Fig. 1i and Supplementary Fig. 12) a stronger white line peak; 2) more hybrid orbitals of Mn 3d and O 2p; 3)



**Fig. 1 | Surface and interface electronic structure characterizations.** **a** The X-ray diffraction patterns; the high-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM) of **(b)**  $\text{SmMn}_2\text{O}_5$  (SMO) and **(c)**  $\text{Mn}_2\text{O}_3/\text{SmMn}_2\text{O}_5$  ( $\text{Mn}_2\text{O}_3/\text{SMO}$ ; A: SMO surface; B: interface; C:  $\text{Mn}_2\text{O}_3$ ); **(d)** the normalized Mn L-edges electron energy loss spectroscopies (EELS) of SMO,  $\text{Mn}_2\text{O}_3\text{-SmMn}_2\text{O}_5$  ( $\text{Mn}_2\text{O}_3\text{-SMO}$ ), and  $\text{Mn}_2\text{O}_3/\text{SMO}$  at the position of A, B, and C; **(e)** Schematic

illustration of the interface interactions on  $\text{Mn}_2\text{O}_3/\text{SMO}$ ; **(f)** the R-space Fourier-transformed FT ( $k^3\chi(k)$ ) of Mn K-edge (extended x-ray absorption fine structure) EXAFS spectra. **(g)** Sm  $L_3$ -edge (X-ray absorption near edge structure) XANES spectra, **(h)** Sm  $3d$  XPS, and **(i)** the normalized O K-edge XANES spectra of SMO,  $\text{Mn}_2\text{O}_3\text{-SMO}$ , and  $\text{Mn}_2\text{O}_3/\text{SMO}$ .

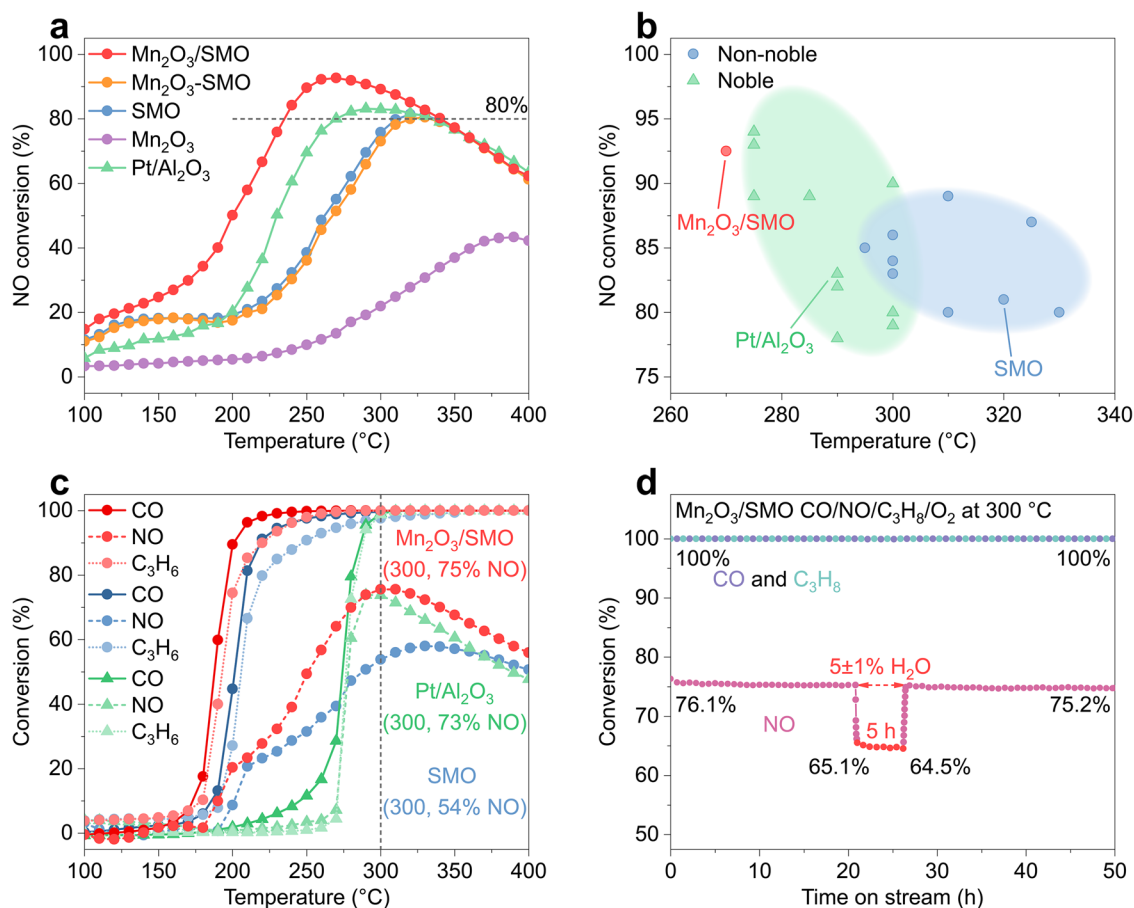
a higher peak intensity ratio of  $\alpha/\gamma$  obtained on  $\text{Mn}_2\text{O}_3/\text{SMO}$ , where the peaks  $\alpha$  and  $\gamma$  represent the Mn  $3d$   $e_g/t_{2g}$  and  $e_g$  orbitals, respectively<sup>36,37</sup>. These Mn L-edge and O K-edge soft-XAS spectra analyses agree well with the Mn L-edge and O K-edge EELS spectra in surface and interface electronic structure of these samples. The EPR spectra further manifest that the exsolved  $\text{Mn}_2\text{O}_3/\text{SMO}$  possesses the most oxygen vacancies among these samples, which stems from the strong interface interactions (Supplementary Fig. 13).

These disparities indicate that  $\text{Mn}_2\text{O}_3/\text{SMO}$  displays a higher covalency of the Mn-O bond because of the strong orbital hybridizations of Mn  $3d$  and O  $2p$ . These observations are complemented by a

comprehensive analysis to gain insights into the electronic structures at the interface between exsolved- $\text{M}_2\text{O}_3$  and SMO. Fundamentally, this interface facilitates effective electron transfer from the exsolved- $\text{Mn}_2\text{O}_3$  to SMO, enhancing the covalency of the Mn-O bond at the  $\text{O}_{\text{lat}}$  adjacent to the  $\text{Mn}^{3+}$  cations (Fig. 1e)<sup>16,17,38</sup>.

### NO oxidation performance

The NO conversions of  $\text{Pt}/\text{Al}_2\text{O}_3$ , SMO,  $\text{Mn}_2\text{O}_3/\text{SMO}$ ,  $\text{Mn}_2\text{O}_3$ , and  $\text{Mn}_2\text{O}_3\text{-SMO}$  catalysts are conducted to analyze the catalytic performance (Fig. 2a). Distinctly paramount among these, the  $\text{Mn}_2\text{O}_3/\text{SMO}$  exhibits superior NO conversion (93%) at 270 °C. The  $T_{80}$  (the onsite



**Fig. 2 | Oxidation activity of diesel exhaust gas. a** NO oxidation activity of Pt/Al<sub>2</sub>O<sub>3</sub>, SmMn<sub>2</sub>O<sub>5</sub> (SMO), Mn<sub>2</sub>O<sub>3</sub>, Mn<sub>2</sub>O<sub>3</sub>/SmMn<sub>2</sub>O<sub>5</sub> (Mn<sub>2</sub>O<sub>3</sub>/SMO), and Mn<sub>2</sub>O<sub>3</sub>-SmMn<sub>2</sub>O<sub>5</sub> (Mn<sub>2</sub>O<sub>3</sub>-SMO). **b** Plot of maximum conversion for NO oxidation vs. temperature for Mn<sub>2</sub>O<sub>3</sub>/SMO, mullite-based catalysts, perovskite-based catalysts,

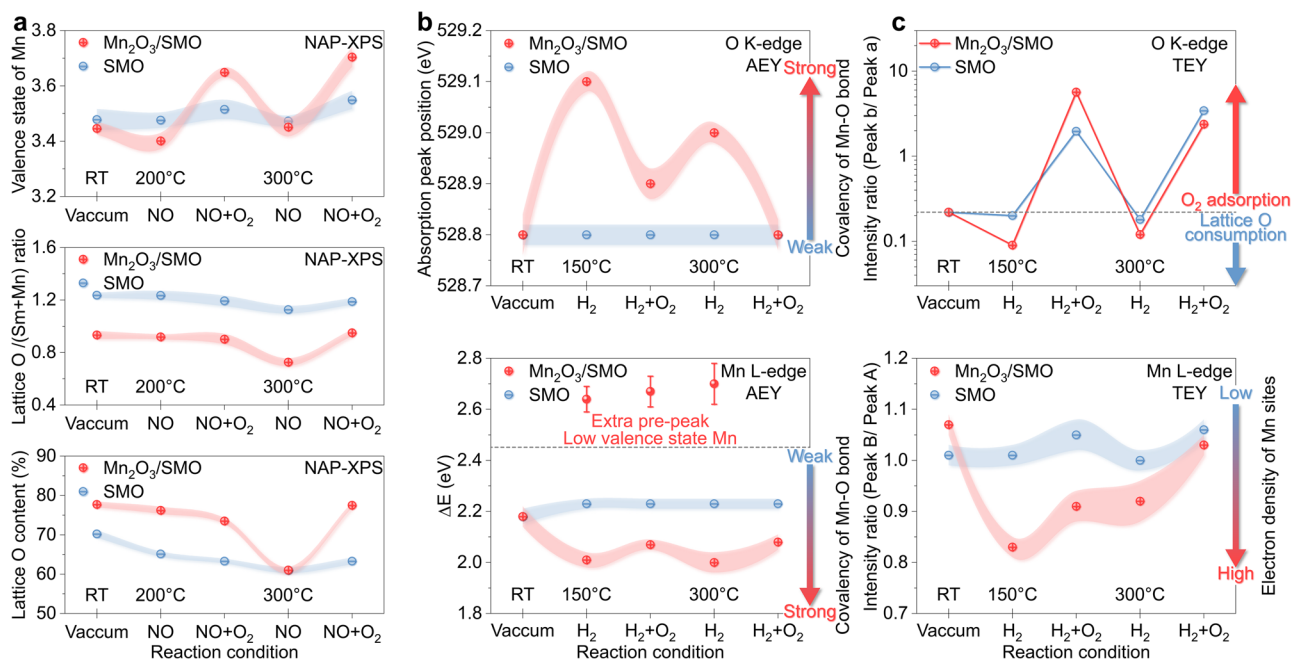
and noble metal catalysts. **c** Diesel oxidation catalyst (DOC) performance of SMO, Mn<sub>2</sub>O<sub>3</sub>/SMO, and Pt/Al<sub>2</sub>O<sub>3</sub>. **d** DOC stability of Mn<sub>2</sub>O<sub>3</sub>/SMO for long-term oxidation reaction at 300 °C. Reaction conditions: 500 ppm NO, 1% CO, 2000 ppm C<sub>3</sub>H<sub>6</sub>, 10% O<sub>2</sub>, 5 ± 1% H<sub>2</sub>O, and balance N<sub>2</sub>.

temperature when NO conversion is higher than 80%) of Mn<sub>2</sub>O<sub>3</sub>/SMO (235 °C) is also 50 and 100 °C lower than that of the Pt/Al<sub>2</sub>O<sub>3</sub> and Mn<sub>2</sub>O<sub>3</sub>-SMO samples. The activity profile of Mn<sub>2</sub>O<sub>3</sub>-SMO is quite similar to that of SMO. This finding underscores the critical roles of the exsolved interface, demonstrating that the exsolved Mn<sub>2</sub>O<sub>3</sub> (Mn<sub>2</sub>O<sub>3</sub>/SMO) rather than the impregnated Mn<sub>2</sub>O<sub>3</sub> (Mn<sub>2</sub>O<sub>3</sub>-SMO) improves the NO oxidation activity of SMO. To better understand the impact of exsolved Mn<sub>2</sub>O<sub>3</sub> on NO oxidation, we have synthesized a variety of exsolved Mn<sub>2</sub>O<sub>3</sub>-supported samples with diverse Mn<sub>2</sub>O<sub>3</sub> content. Incrementing the Mn<sub>2</sub>O<sub>3</sub> content does not contribute much to the activity of NO oxidation (Supplementary Fig. 14). Combined with the results of structure characterizations, the active sites in Mn<sub>2</sub>O<sub>3</sub>/SMO are mainly at the surface/interface of the SMO and the key role of the Mn<sub>2</sub>O<sub>3</sub> species is to tune the surface/interface electronic structure of the SMO. It is also discovered that Mn<sub>2</sub>O<sub>3</sub>/SMO maintains the greatest activity across the component range because of the higher interface oxygen defect concentrations. This provides a reasonable deduction that the main active sites of Mn<sub>2</sub>O<sub>3</sub>/SMO are located primarily at the interface instead of surface Mn<sub>2</sub>O<sub>3</sub>.

In order to obtain a comparative measurement of activity, a graph representing the correlation between maximum NO conversion and temperatures for previously reported catalysts (with/without noble metals) is summarized (Fig. 2b). Mn<sub>2</sub>O<sub>3</sub>/SMO still manifests a supreme performance as it functions at a substantially lower reaction temperature and demonstrates a higher maximum NO conversion compared to both noble metal<sup>39–45</sup> and transition metal-oxide

(perovskite<sup>3,34,46</sup> and mullite<sup>2,17,27,30,47</sup>) counterparts. In addition, we also tested the DOC performance in terms of CO, C<sub>3</sub>H<sub>6</sub>, and NO subjected to laboratory-simulated diesel exhaust conditions (Fig. 2c). Mn<sub>2</sub>O<sub>3</sub>/SMO still exhibits superior activities in the oxidations of CO, C<sub>3</sub>H<sub>6</sub>, and NO as compared to Pt/Al<sub>2</sub>O<sub>3</sub> and Mn<sub>2</sub>O<sub>3</sub>-SMO<sup>17</sup>. Fig. 2d shows the higher durability and water vapor resistance (Supplementary Fig. 15) of Mn<sub>2</sub>O<sub>3</sub>/SMO in 50 h, as well as excellent thermal stability at 800 °C aging for 10 h (Supplementary Fig. 16). We have also coated the slurry of Mn<sub>2</sub>O<sub>3</sub>/SMO on a honeycomb Cordierite-support and tested its DOC performance (Supplementary Fig. 17). The DOC performance of the honeycomb samples can meet the DOC standards of China Environmental Protection Industry Association (T/CAEPI 12.1-2017). This reinforces the superior robustness and functionality of Mn<sub>2</sub>O<sub>3</sub>/SMO, as well as the simple preparation method, making it one a promising candidate as a DOC catalyst.

To further align with realistic operational conditions in diesel vehicles, a CO<sub>2</sub> concentration of around 8% and H<sub>2</sub>O at around 8% as well as thermal aging resistance are necessary to pretreat the catalyst before evaluating the catalytic performance of SMO and Mn<sub>2</sub>O<sub>3</sub>/SMO (Supplementary Fig. 18)<sup>48</sup>. Mn<sub>2</sub>O<sub>3</sub>/SMO displays better catalytic activity for NO oxidation (71.8% conversion at 325 °C), CO oxidation (100% conversion at 300 °C), C<sub>3</sub>H<sub>6</sub> oxidation (100% conversion at 300 °C) than SMO (100% CO and 99.4% C<sub>3</sub>H<sub>6</sub> conversions at 300 °C and 58.1% NO conversion at 350 °C). The tested data demonstrate the application prospect of the exsolved Mn<sub>2</sub>O<sub>3</sub>/SMO catalyst for exhaust oxidation treatment. In addition, we also measured the DOC durability of the



**Fig. 3 | Dynamic structure evolutions of lattice O and metal Mn sites.** **a** Dynamic evolutions of Mn valence state in *NAP-XPS* results,  $O_{\text{latt}}/(\text{Sm}+\text{Mn})$  ratio and lattice oxygen ( $O_{\text{latt}}$ ) content of Mn<sub>2</sub>O<sub>3</sub>/SmMn<sub>2</sub>O<sub>5</sub> (Mn<sub>2</sub>O<sub>3</sub>/SMO) and SmMn<sub>2</sub>O<sub>5</sub> (SMO) in NO oxidation; dynamic evolutions of covalency of the Mn-O bond and Mn *3d*

orbitals at the Mn sites of Mn<sub>2</sub>O<sub>3</sub>/SMO and SMO in *NAP-XAS* results of **(b)** AEY and **(c)** TEY modes. These error bars are mainly derived from fitting, reading, and random errors of experimental data.

exsolved Mn<sub>2</sub>O<sub>3</sub>/SMO catalyst for 64 h under the conditions of 8% CO<sub>2</sub> and 8% H<sub>2</sub>O (Supplementary Fig. 19). 8% water vapor can decrease the catalytic oxidation property (56.9% NO conversion), which stems from the competitive adsorption of water vapor at the active sites. When water vapor is removed from reaction system, the catalytic activity of Mn<sub>2</sub>O<sub>3</sub>/SMO becomes better (73% NO conversion) and keeps the long-term durability for 15 h. Then, the 8% water vapor is pumped into the reactor again, the catalytic performance is the same as for the last water vapor condition (56.9% NO conversion). After removing the water vapor, the catalytic activity rapidly restores to the original level before secondly adding water vapor (73% NO conversion) and the system remains unchanged for the next 10 h. The initial tests of 20 h under NO, CO, C<sub>3</sub>H<sub>6</sub>, O<sub>2</sub>, H<sub>2</sub>O, CO<sub>2</sub>, and N<sub>2</sub> belong to the pre-treatment process of catalysts. According to the standard practices of DOCS, these catalysts are aged at 750 °C for 50 h with 10% concentration of water vapor. After pretreatment, the catalytic oxidation reaction measurements of these aged catalysts are further conducted under the conditions of a large amount of water vapor ( $\geq 8\%$ ) and CO<sub>2</sub> ( $\geq 8\%$ ) (Supplementary Fig. 20). The exsolved Mn<sub>2</sub>O<sub>3</sub>/SMO shows the higher performance for NO, CO, and C<sub>3</sub>H<sub>6</sub> oxidation than the SMO and commercial Pt/Al<sub>2</sub>O<sub>3</sub>. At 325 °C, CO, NO, and C<sub>3</sub>H<sub>6</sub> conversions of the Mn<sub>2</sub>O<sub>3</sub>/SMO are 100%, 62.6%, and 100%, respectively.

### Dynamic evolutions of $O_{\text{latt}}\text{-Mn}^{3+}$ sites

In order to elucidate the dynamic evolutions of the valence state of Mn and reactivity of  $O_{\text{latt}}$  in NO oxidation, *NAP-XPS* spectra of Mn<sub>2</sub>O<sub>3</sub>/SMO and SMO were employed. The O *1s* and Mn *2p* XPS spectra of Mn<sub>2</sub>O<sub>3</sub>/SMO display significant peak shifts to higher binding energy in O *1s* and to lower binding energy in Mn *2p* under both NO and NO + O<sub>2</sub> atmospheres at 200 and 300 °C (Supplementary Fig. 21). In comparison, the SMO shows trivial changes in NO adsorption and oxidation processes. To further investigate the dynamic changes, we derived the variation curves of the valence state of Mn and  $O_{\text{latt}}$  content *versus* the reaction conditions by calculating the fitting data of Mn *2p* and O *1s* XPS spectra (Supplementary Figs. 22–41). There is a slight decrease in

the average valence state of Mn (Fig. 3a) and a consequent increase of adsorbed oxygen content (Supplementary Fig. 42) on the SMO surface at 200 °C, however, the lattice oxygen position and  $O_{\text{latt}}/(\text{Sm}+\text{Mn})$  does not change during the process (Fig. 3a and Supplementary Fig. 43). The results suggest that the surface  $O_{\text{latt}}$  species on SMO have poor reactivity in NO oxidation and that NO gas mainly adsorbs at the SMO surface at low temperature. When O<sub>2</sub> is also introduced at 200 °C, a weak increase in the valence state of Mn is observed, which can be attributed to the partial oxidation of NO and stored on SMO at Mn sites. The position of  $O_{\text{latt}}$  still fails to respond to NO and O<sub>2</sub> even at 300 °C. The results suggest that traditional Mn sites are only active, the  $O_{\text{latt}}$  sites of SMO hardly participate in NO adsorption and oxidation reaction below 300 °C. As for Mn<sub>2</sub>O<sub>3</sub>/SMO, when NO is introduced, the position of  $O_{\text{latt}}$  slightly shifts to lower binding energy and there is a decrease in the ratio of  $O_{\text{latt}}/O_{\text{ads}}$  and  $O_{\text{latt}}/(\text{Sm}+\text{Mn})$ ; at the same time, the valence state of Mn also decreases (Fig. 3a). The results indicate that the  $O_{\text{latt}}$  sites considerably react with NO even at 200 °C, which leads to the electron transfer from NO to Mn via the covalent bond of  $O_{\text{latt}}\text{-Mn}^{3+}$ . When O<sub>2</sub> is also introduced at 200 °C, the valence state of Mn is even higher than that under vacuum conditions (surface oxidation process), and the position of  $O_{\text{latt}}$  moves back to its original binding energy, suggesting that the reacted  $O_{\text{latt}}\text{-Mn}^{3+}$  groups undergo a regeneration process by the O<sub>2</sub> dissociation at oxygen vacancies (Supplementary Fig. 43).

On increasing the temperature, the reactivity of  $O_{\text{latt}}$  also increases because of increased changes in NO and NO + O<sub>2</sub> atmospheres. One should note that there is an imbalance between the Mn valence state and the  $O_{\text{latt}}$  quantity in the regeneration process, namely that Mn in Mn<sub>2</sub>O<sub>3</sub>/SMO has a higher valence state and  $O_{\text{latt}}$  has a lower position, whereas the oxidation state of the Mn atoms in SMO increases and the  $O_{\text{latt}}$  position remains unchanged. This can be due to the enhancement of oxygen adsorption, dissociation, and exchange. At 300 °C, the consumption rate of  $O_{\text{latt}}$  on Mn<sub>2</sub>O<sub>3</sub>/SMO is even larger than the compensation rate. The dynamic evolutions from *NAP-XPS* confirm that the  $O_{\text{latt}}$  sites on Mn<sub>2</sub>O<sub>3</sub>/SMO act as the primary active sites in NO

oxidation. Moreover, we also directly observed that the surface Sm content (Sm/Mn ratio) in SMO increases when increasing the reaction temperature, whereas the surface Sm content in Mn<sub>2</sub>O<sub>3</sub>/SMO decreases (Supplementary Fig. 44). Large-ion-radius Sm cations on Mn<sub>2</sub>O<sub>3</sub>/SMO contribute to preserve its mullite crystal structure and tune the interface interactions, but they are the inactive as metal sites in NO oxidation (Supplementary Figs. 45, 46). Thus, the SMO catalyst shows poor durability during the catalytic oxidation process due to surface Sm enrichment, whereas the Mn<sub>2</sub>O<sub>3</sub>/SMO catalyst possesses excellent durability owing to surface Mn enrichment.

We further summarize the transfer process of oxygen species on the Mn<sub>2</sub>O<sub>3</sub>/SMO surface in the cooperative MvK mechanism. Traditional SMO catalysts mainly comply with the E-R mechanism, where adsorbed oxygen species at the Mn sites react with NO gas and are converted into adsorbed nitrates. Differently, for Mn<sub>2</sub>O<sub>3</sub>/SMO there exists a strong electron transfer between two phases, which efficiently activates the surface O<sub>latt</sub> sites. Mn<sub>2</sub>O<sub>3</sub>/SMO has obvious changes in lattice oxygen and adsorbed oxygen species at 300 °C (Fig. 3a and Supplementary Figs. 42, 43). Under a NO atmosphere, NO gas reacts with lattice oxygen into adsorbed nitrate and nitrite species, where lattice oxygen is consumed and are not compensated. The Mn valence state in Mn<sub>2</sub>O<sub>3</sub>/SMO also has a distinct decrease. When NO and O<sub>2</sub> are introduced, lattice oxygen is dynamically consumed and regenerated. The lattice oxygen position does not restore the original peak position, but the valence state of the Mn atoms has a strong increase (Fig. 3a). These results indicate that the lattice oxygen consumption rate of Mn<sub>2</sub>O<sub>3</sub>/SMO is faster than regeneration rate at 300 °C. Therefore, Mn<sub>2</sub>O<sub>3</sub>/SMO complies with the dominated MvK mechanism and to a lesser degree the E-R mechanism. The oxygen transfer process with the Mn<sub>2</sub>O<sub>3</sub>/SMO catalyst mainly occurs at the Mn sites and oxygen vacancies. Introduction of oxygen makes nitrites and nitrates easily desorbed from the surface due to the oxidative environment.

As a complementary technology to NAP-XPS spectra (1–4 nm), NAP-XAS spectra usually provide a shallower surface probe depth (1–3 nm in Auger electron yield (AEY) mode). It can be used to identify the chemical descriptors such as covalency of metal-oxygen bond and electron density by examining the electron transition probability at various orbitals under different reaction conditions<sup>49,50</sup>. To monitor the dynamic evolutions on surface electronic structure at O<sub>latt</sub> and Mn sites, we employed NAP-XAS spectra of the O K-edge and Mn L-edge using the total electron yield (TEY) and AEY modes (Supplementary Figs. 47–54), respectively. As known, the AEY mode is more surface-sensitive than the TEY mode, and it includes more detailed covalency information of the metal-oxide bond, while the TEY mode includes information about the O<sub>2</sub> adsorption and electron density of cations<sup>37</sup>. The covalency of the Mn-O bond is confirmed by the peak of Mn 3d-O 2p hybrid orbitals at the O K-edge at around 529 eV and the peak distance ( $\Delta E$ ) for the Mn L<sub>3</sub>-edge in 641–644 eV. In the AEY mode, the covalency of the Mn-O bond on SMO (Fig. 3b) is inactive under both reduced and oxidized atmospheres. In contrast, Mn<sub>2</sub>O<sub>3</sub>/SMO exhibits a distinct enhancement in the covalency of the Mn-O bond under a reduced atmosphere, and an additional shoulder peak in the Mn L<sub>3</sub>-edge spectra at around 640 eV occurred (Supplementary Fig. 52). The results suggest that surface O<sub>latt</sub> shows high activity in the process of bonding with H\* radicals and reduction of Mn sites, leading to the increase of Mn 3d empty orbitals. When O<sub>2</sub> was introduced, it could adsorb at Mn sites and partially heal the oxygen vacancies at 150 °C, resulting in the decrease of covalency of the Mn-O bond. One should note that the position of O<sub>latt</sub> under a H<sub>2</sub> atmosphere at 300 °C is still lower than that at 150 °C, which can be due to the influence of temperature on the O<sub>latt</sub> migration. Under oxidized conditions at 300 °C, O<sub>2</sub> can almost fill nearly all the oxygen vacancies, restoring the pristine covalency of the Mn-O bond under vacuum.

The TEY mode of O K-edge and Mn L-edge XAS spectra is used to describe the O<sub>2</sub> adsorption and electron density (Fig. 3c). The O<sub>2</sub>

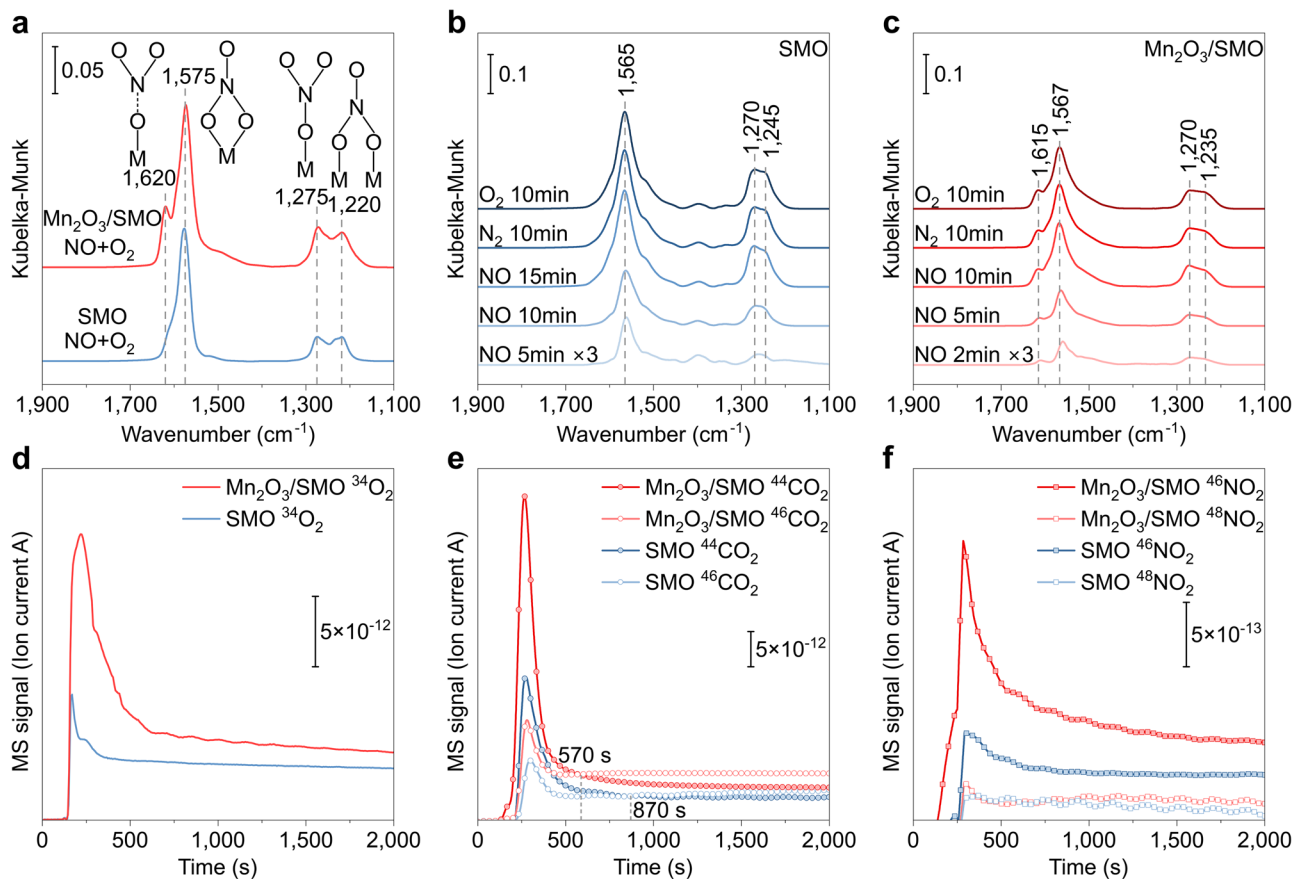
adsorption intensity is calculated using the peak intensity ratios of the first two peaks,  $\alpha$  and  $\beta$ , in the O K-edge XAS spectra, while the electron density is calculated using the peak intensity ratios of two peaks, A and B, in the Mn L<sub>3</sub>-edge. The electron density of SMO at the Mn sites slightly changes under redox cycles, while O<sub>2</sub> can adsorb and dissociate at the Mn sites of SMO, leading to a decrease in the electron density of the Mn sites. Whereas Mn<sub>2</sub>O<sub>3</sub>/SMO exhibits a considerable increase in electron density of Mn sites under an H<sub>2</sub> atmosphere, especially at 150 °C, and the behavior of O<sub>2</sub> adsorption and electron density of Mn sites under O<sub>2</sub> atmosphere at 300 °C are similar to SMO. The results suggest that the Mn sites of Mn<sub>2</sub>O<sub>3</sub>/SMO are still less active at 300 °C, consistent with the H<sub>2</sub>-TPR results. The time-resolved MS signals of H<sub>2</sub>O also confirm the redox cycles (Supplementary Fig. 55). It is found that the active sites on Mn<sub>2</sub>O<sub>3</sub>/SMO are dominated by O<sub>latt</sub> sites, whereas on SMO, it is the traditional Mn sites. The active order shows accordance with that in NO oxidation at 150 and 300 °C. The above NAP-XPS and NAP-XAS results directly demonstrate the temperature-dependent changes in the valence state of Mn and the covalency of the Mn-O bond and further validate the roles of O<sub>latt</sub> at the interface between exsolved-Mn<sub>2</sub>O<sub>3</sub> and mullite support.

### Key intermediate species in NO oxidation

To gain insights into intermediates in NO oxidation, in-situ diffuse reflectance infrared Fourier transformations spectroscopy (DRIFTS) spectra were recorded for Mn<sub>2</sub>O<sub>3</sub>/SMO and SMO under NO and NO + O<sub>2</sub> conditions (Fig. 4a–c and Supplementary Fig. 56). The peak intensity of the IR spectra was converted into Kubelka-Munk units to analyze the concentration variations of intermediates. The observed bands at 1235, 1270, and 1570 cm<sup>-1</sup> correspond to the bridged, monodentate, and bidentate nitrate species, respectively<sup>16,17</sup>. In addition, the band at 1615 cm<sup>-1</sup> is assigned to the weakly adsorbed NO<sub>2</sub> at O<sub>latt</sub> sites (O<sub>latt</sub>-NO<sub>2</sub>) as the nitrite species<sup>510</sup>. Mn<sub>2</sub>O<sub>3</sub>/SMO exhibits a stronger IR peak signal for nitrate species compared to SMO under NO + O<sub>2</sub> at 200 °C (Fig. 4a), indicating the superior NO adsorption ability of Mn<sub>2</sub>O<sub>3</sub>/SMO. Mn<sub>2</sub>O<sub>3</sub>/SMO possesses more monodentate nitrates than SMO. In addition, we observed an increase in the amount of adsorbed NO<sub>2</sub> (1615 cm<sup>-1</sup>, nitrite species) at active O<sub>latt</sub> sites of Mn<sub>2</sub>O<sub>3</sub>/SMO. Desorption of nitrites and monodentate nitrates to NO<sub>2</sub> is known to be more facile than the bridged nitrate<sup>17</sup>. Mn<sub>2</sub>O<sub>3</sub>/SMO exhibits rapid NO oxidation activation on the surface due to the larger peak intensity variations compared to SMO (Fig. 4b–c). When O<sub>2</sub> is introduced, the amount of monodentate nitrate in Mn<sub>2</sub>O<sub>3</sub>/SMO distinctly decreases and the bidentate and bridged nitrate species show slight decreases. However, the adsorbed NO<sub>2</sub> at O<sub>latt</sub> sites (nitrite species) of Mn<sub>2</sub>O<sub>3</sub>/SMO increased<sup>17,34</sup>. The result demonstrates the transformation from the nitrates to nitrites during oxygen-rich NO oxidation.

The N 1s NAP-XPS spectra (Supplementary Figs. 57, 58) confirm that NO gas preferred to adsorb at the O<sub>latt</sub> sites of Mn<sub>2</sub>O<sub>3</sub>/SMO, and its intermediates contain extra O<sub>site</sub>-NO and O<sub>site</sub>-NO<sub>2</sub> species compared to traditional SMO. The adsorbed NO on O<sub>latt</sub> can transform into nitrite species and oxygen vacancy (-O<sub>latt</sub>-NO<sub>2</sub>-Mn-O<sub>v</sub>), and the chemical bond for O<sub>latt</sub>-N can be broken into NO<sub>2</sub>. The SMO catalyst mainly complies with the E-R mechanism, where adsorbed oxygen species react with NO gas into nitrate species, such as monodentate, bidentate, bridged nitrates. Different from SMO, Mn<sub>2</sub>O<sub>3</sub>/SMO depends on the dominated MvK mechanism and to a lesser extent the E-R mechanism. NO gas preferentially adsorbs on lattice oxygen sites and produces the extra nitrite species (O<sub>site</sub>-NO<sub>2</sub>). The nitrites on the lattice oxygen can more easily desorb from the catalyst surface compared to traditional nitrate species. These results highlight that the higher NO oxidation activity of Mn<sub>2</sub>O<sub>3</sub>/SMO stems from the quick decomposition or desorbed process of nitrite species and monodentate nitrates to NO<sub>2</sub>.

To clarify the water effect mechanism on mullite oxides in NO oxidation, we investigated in-situ DRIFTS spectra under the atmosphere of NO + O<sub>2</sub> + H<sub>2</sub>O at 200 °C (Supplementary Fig. 59). The



**Fig. 4 | Active sites and reaction mechanisms in NO oxidation.** **a** In-situ diffuse reflectance infrared Fourier transform spectroscopy (DRIFTS) of Mn<sub>2</sub>O<sub>3</sub>/SmMn<sub>2</sub>O<sub>5</sub> (Mn<sub>2</sub>O<sub>3</sub>/SMO) and SmMn<sub>2</sub>O<sub>5</sub> (SMO) under NO + O<sub>2</sub> at 200 °C. Time-resolved in-situ DRIFTS spectra of the **(b)** SMO and **(c)** Mn<sub>2</sub>O<sub>3</sub>/SMO under NO gas at 200 °C. **d** Time-resolved isotopic <sup>36</sup>O<sub>2</sub> exchange reaction at 300 °C. **(e)** time-resolved isotopic <sup>36</sup>O<sub>2</sub> labeled online MS for CO oxidation at 150 °C, **(f)** time-resolved isotopic <sup>36</sup>O<sub>2</sub> labeled online MS for NO oxidation at 300 °C.

intermediates formed over the SMO and Mn<sub>2</sub>O<sub>3</sub>/SMO catalysts are described in Supplementary Table 2. The IR vibration intensity of water over the SMO catalyst (water at 1625 cm<sup>-1</sup> and hydroxyl in 3400–3700 cm<sup>-1</sup>) is far stronger than that over Mn<sub>2</sub>O<sub>3</sub>/SMO (1647 cm<sup>-1</sup> and 3400–3700 cm<sup>-1</sup>), indicating that the SMO surface is covered by water molecules and a stronger competitive adsorption exists with reactant gases than does for Mn<sub>2</sub>O<sub>3</sub>/SMO (Supplementary Fig. 59). The IR peak at 1625 cm<sup>-1</sup> can be attributed to adsorbed nitrite species (Supplementary Table 2). If it is nitrite species, this will confirm that water is mainly adsorbed at the Mn active sites of the SMO catalyst and the competitive adsorption makes the NO oxidation comply more with the MvK mechanism at the O<sub>latt</sub> sites. Therefore, the water poisoning mainly originates from the competitive adsorption and the desorbed NO<sub>3</sub><sup>-</sup> species binding with water. The observed monodentate nitrate and nitrite species demonstrate the E-R mechanism at the Mn site and cooperative MvK mechanism at O<sub>latt</sub> site in NO oxidation, respectively. These two reaction mechanisms are negatively affected by water vapor through the competitive adsorption and desorbed nitrates.

DFT calculations were conducted to further elucidate the impacts of O<sub>latt</sub> sites in NO oxidation and NO<sub>2</sub> desorption (Supplementary Fig. 60). The models are constructed based on the experimental results and previous reports<sup>10,27,33</sup>. The O-Mn<sup>4+</sup> of the SMO model exhibits a higher energy barrier of 2.79 eV in NO oxidation (E1) at the O<sub>latt</sub> sites. However, the O-Mn<sup>3+</sup> of the SMO model in E1 is lower (1.45 eV), whereas the O-Mn<sup>3+</sup> of the Mn<sub>2</sub>O<sub>3</sub>/SMO model is even lower at 0.56 eV. The results confirm that O-Mn<sup>3+</sup> of Mn<sub>2</sub>O<sub>3</sub>/SMO is the major active site in NO oxidation. Oxygen vacancy formation energies of

interface Mn<sup>3+</sup>-O<sub>site</sub> in Mn<sub>2</sub>O<sub>3</sub>/SMO, Mn<sup>3+</sup>-O<sub>site</sub> in SMO, and Mn<sup>4+</sup>-O<sub>site</sub> in SMO also agree with the above calculations, where they are -1.1 eV, -1.8 eV and -2.7 eV, respectively. In addition, the NO<sub>2</sub> desorption (O<sub>latt</sub>-NO<sub>2</sub> species) on the O-Mn<sup>3+</sup> of Mn<sub>2</sub>O<sub>3</sub>/SMO and SMO are exothermic processes (-0.68 and -0.50 eV), while it is an endothermic process (0.11 eV) on the O-Mn<sup>4+</sup> of SMO. The results indicate that NO<sub>2</sub> is more easily desorbed from the O-Mn<sup>3+</sup> sites, which is aligned well with the in-situ spectroscopy results.

The time-resolved isotopic <sup>36</sup>O<sub>2</sub> exchange experiments are measured to demonstrate the activity of lattice oxygen (Fig. 4d). Each sample was pretreated at 300 °C for 3 h under an Ar atmosphere to decrease surface adsorbed oxygen. It was revealed that Mn<sub>2</sub>O<sub>3</sub>/SMO exhibits higher O<sub>latt</sub> activation and dissociation abilities compared to SMO because of the stronger <sup>34</sup>O<sub>2</sub> signals of Mn<sub>2</sub>O<sub>3</sub>/SMO versus those of SMO. To investigate the activity of O<sub>latt</sub> sites, we use CO and isotopic <sup>36</sup>O<sub>2</sub> as the probe molecules at 150 °C. To further investigate the activation and dissociation ability of molecular oxygen, the transient oxygen exchange test was conducted at different temperatures. Wachsmann et al. proposed that the exchange of lattice oxygen (<sup>34</sup>O<sub>2</sub>) on non-stoichiometric metal oxides is usually better at oxygen dissociation when using 1:1 isotopic mixture<sup>51,52</sup>. By analyzing the concentration variations of oxygen exchange (Supplementary Figs. 61, 62), we demonstrate that the oxygen exchange rate of Mn<sub>2</sub>O<sub>3</sub>/SMO is distinctly higher than that of SMO at the same temperature. At 300 °C, the Mn<sub>2</sub>O<sub>3</sub>/SMO shows the better oxygen activation ability, while the oxygen exchange rate of SMO is very low. The results are consistent with the NAP-XPS spectra and previous work on perovskites<sup>51,52</sup>.

Furthermore, we also calculated the apparent activation energy of  $O_2$  for the two catalysts by the slope of Arrhenius plot. The apparent oxygen activation energy of SMO and  $Mn_2O_3/SMO$  catalysts are 38.8 and 44.8 kJ/mol, respectively.

Both the MvK and E-R mechanisms exist in the  $Mn_2O_3/SMO$  catalyst (Fig. 4e), as indicated by the simultaneous appearance of  $^{44}CO_2$  and  $^{46}CO_2$  signals. Interestingly,  $Mn_2O_3/SMO$  exhibits an earlier crossing time (570 s) in the  $^{44}CO_2$  and  $^{46}CO_2$  signals compared to SMO (870 s), with a stronger initial intensity of  $^{44}CO_2$ . This suggests that the consumption rate of  $O_{latt}$  with CO in  $Mn_2O_3/SMO$  is much higher than that in SMO. On decreasing the temperature to 100 °C (Supplementary Fig. 63), the  $O_{latt}$  activity in  $Mn_2O_3/SMO$  weakens, and no crossing point is observed during the 2400 s. However, the signal of  $^{44}CO_2$  is still stronger than that of  $^{46}CO_2$ . Therefore, the CO oxidation on  $Mn_2O_3/SMO$  mainly follows the MvK mechanism and  $O_{latt}$  is the important active site. Furthermore, the time-resolved isotopic  $^{36}O_2$  signal at 300 °C (Fig. 4f) shows that the  $Mn_2O_3/SMO$  exhibits a much stronger  $^{46}NO_2$  signal compared to SMO, while the intensities of  $^{48}NO_2$  signal are nearly the same, indicating that the reaction rate at the Mn sites of  $Mn_2O_3/SMO$  is low and similar to that of SMO (the E-R mechanism). In contrast, the reaction rate at the  $O_{latt}$  sites is significantly improved on  $Mn_2O_3/SMO$ , and the NO oxidation pathway is determined by the MvK mechanism.

The reaction orders of  $Mn_2O_3/SMO$  and SMO were calculated to achieve strict kinetic control (Supplementary Table 3). The reaction orders of SMO for NO and  $O_2$  are 0.61 and 0.59, respectively, while a noticeable decrease of  $Mn_2O_3/SMO$  is observed (0.55 to NO and 0.47 to  $O_2$ ). As known, lower reaction orders to  $O_2$  typically indicate that adsorbed oxygen can be easily activated at a catalyst surface with oxygen vacancies<sup>53</sup>. That is, decomposition of  $O_2$  is more facile at the surface of  $Mn_2O_3/SMO$ . In addition, the decrease in NO reaction orders can be attributed to the strong competitive adsorption of  $O_2$  to NO. As demonstrated through in-situ spectroscopy results, the  $Mn_2O_3/SMO$  catalyst presents both higher covalency of Mn–O bond and electron density of Mn sites, which leads to the generation of more  $O_{latt}$  sites. These  $O_{latt}$  sites facilitate the activities of NO oxidation dominated by the cooperative MvK mechanism.

## Discussion

We have prepared a highly active DOC catalyst whereby  $Mn_2O_3$  is exsolved from mullite surface by a facile nonstoichiometric exsolution method. By a series of in-situ spectroscopies, we elucidate the role and dynamic evolutions of lattice oxygen, serving as the predominant active sites, in NO oxidation. Different from the traditional mullite catalyst, lattice oxygen adjacent to  $Mn^{3+}$  cations at the interface between exsolved- $Mn_2O_3$  and the support displays strong covalency of Mn–O bond and electron enrichment at the Mn sites. In both model reactions under redox cycles and NO oxidations, these  $O_{latt}$  sites are largely involved in these reactions, exhibiting more significant changes in the valence state of Mn and covalency of the Mn–O bond. Compared to the Eley-Rideal mechanism on the  $Mn^{4+}$  cations of mullite, this catalyst follows the characteristic of cooperative Mars-van Krevelen mechanism operating at lattice oxygen sites. The enhanced reaction rates are owing to the lower energy barriers of NO oxidation with lattice oxygen (monodentate nitrates and nitrites) and an exothermic process of  $NO_2$  desorption from the surface. Moreover, the leaving oxygen vacancies can be easily healed by  $O_2$  dissociation to form new  $O_{latt}$  sites. Due to the ultra-stable mullite framework and the completion of  $MnO_x$  phase transition process at 800 °C ( $Mn_2O_3$  yield), the  $Mn_2O_3/SMO$  shows higher activity in NO oxidation (93% at 270 °C), surpassing previously reported Pt-based and mullite-based catalysts (86% at 290 °C and 83% at 300 °C). In addition, it also exhibits an excellent DOC performance under the environment of 8%  $CO_2$  and 8%  $H_2O$ . After 50 h hydrothermal aging at 750 °C with a 10%  $H_2O$

concentration, the aged  $Mn_2O_3/SMO$  catalyst still retains 62.6% conversion for NO and 100% conversions for CO and  $C_3H_6$  at 325 °C.

This work underlines three pivotal factors in understanding the roles of  $O_{latt}$  sites: (1) the electron exchanges between exsolved- $Mn_2O_3$  and mullite support, resulting in the formation of more active  $O_{latt}-Mn^{3+}$  local structures, (2) the incorporation of hybrid orbitals of Mn  $3d$  and O  $2p$ , which amplifies the covalency of the Mn–O bond, and (3) the interface and defect induced lattice contractions on the mullite support. These findings advance our comprehension of lattice oxygen behavior, forging a new avenue in the design of metal-oxide-based catalysts. This work will push the frontiers of academic research and the practical applications in the heterogeneous catalysis realm.

## Methods

Experiment and Methods are shown in the Supplementary Information.

## Data availability

Source data are provided with this paper. The authors declare that the data supporting the findings of this study are available within the paper, its supplementary information files, and the Figshare repository. Source data are provided with this paper.

## References

1. Anenberg, S. C. et al. Impacts and mitigation of excess diesel-related  $NO_x$  emissions in 11 major vehicle markets. *Nature* **545**, 467–471 (2017).
2. Wang, W. et al. Mixed-phase oxide catalyst based on Mn-mullite ( $Sm, Gd$ ) $Mn_2O_5$  for NO oxidation in diesel exhaust. *Science* **337**, 832–835 (2012).
3. Kim, C. H., Qi, G., Dahlberg, K. & Li, W. Strontium-doped perovskites rival platinum catalysts for treating  $NO_x$  in simulated diesel exhaust. *Science* **327**, 1624–1627 (2010).
4. Hoang, S. et al. Activating low-temperature diesel oxidation by single-atom Pt on  $TiO_2$  nanowire array. *Nat. Commun.* **11**, 1062 (2020).
5. Wang, F. et al. Ultralow-temperature  $NO_x$  reduction over  $SmMn_2O_5$  mullite catalysts via modulating the superficial dual-functional active sites. *ACS Catal.* **12**, 7622–7632 (2022).
6. Russell, A. & Epling, W. S. Diesel oxidation catalysts. *Catal. Rev.* **53**, 337–423 (2011).
7. Kothari, M. et al. Platinum incorporation into titanate perovskites to deliver emergent active and stable platinum nanoparticles. *Nat. Chem.* **13**, 677–682 (2021).
8. Nie, L. et al. Activation of surface lattice oxygen in single-atom Pt/ $CeO_2$  for low-temperature CO oxidation. *Science* **358**, 1419–1423 (2017).
9. Kunwar, D. et al. Investigating anomalous growth of platinum particles during accelerated aging of diesel oxidation catalysts. *Appl. Catal. B* **266**, 118598 (2020).
10. Zheng, Y. et al. Stable and active oxidation catalysis by cooperative lattice oxygen redox on  $SmMn_2O_5$  mullite surface. *J. Am. Chem. Soc.* **141**, 10722–10728 (2019).
11. Ulissi, Z. W., Medford, A. J., Bligaard, T. & Nørskov, J. K. To address surface reaction network complexity using scaling relations machine learning and DFT calculations. *Nat. Commun.* **8**, 14621 (2017).
12. Medford, A. J. et al. From the Sabatier principle to a predictive theory of transition-metal heterogeneous catalysis. *J. Catal.* **328**, 36–42 (2015).
13. Schlögl, R. Heterogeneous catalysis. *Angew. Chem. Int. Ed.* **54**, 3465–3520 (2015).
14. Shen, Y., Deng, J., Han, L., Ren, W. & Zhang, D. Low-temperature combustion of toluene over Cu-doped  $SmMn_2O_5$  mullite catalysts



- via creating highly active  $\text{Cu}^{2+}$ -O-Mn $^{4+}$  sites. *Environ. Sci. Technol.* **56**, 10433–10441 (2022).
15. Simbock, J. et al. Electronic parameters in cobalt-based perovskite-type oxides as descriptors for chemocatalytic reactions. *Nat. Commun.* **11**, 652 (2020).
  16. Yang, Q. et al. Surface tailoring on  $\text{SrMnO}_3$ @ $\text{SmMn}_2\text{O}_5$  for boosting the performance in diesel oxidation catalyst. *Appl. Catal. B* **320**, 121993 (2023).
  17. Yang, Q. et al. Surface Reconstruction of a mullite-type catalyst via selective dissolution for NO oxidation. *ACS Catal.* **11**, 14507–14520 (2021).
  18. Meng, F. et al. Essential role of lattice oxygen in methanol electrochemical refinery toward formate. *Sci. Adv.* **9**, eadh9487 (2023).
  19. Jacobs, R., Mayeshiba, T., Booske, J. & Morgan, D. Material discovery and design principles for stable, high activity perovskite cathodes for solid oxide fuel cells. *Adv. Energy Mater.* **8**, 1702708 (2018).
  20. Mueller, D. N., Machala, M. L., Bluhm, H. & Chueh, W. C. Redox activity of surface oxygen anions in oxygen-deficient perovskite oxides during electrochemical reactions. *Nat. Commun.* **6**, 6097 (2015).
  21. Grimaud, A. et al. Activation of surface oxygen sites on an iridium-based model catalyst for the oxygen evolution reaction. *Nat. Energy* **2**, 16189 (2016).
  22. Grimaud, A. et al. Activating lattice oxygen redox reactions in metal oxides to catalyse oxygen evolution. *Nat. Chem.* **9**, 457–465 (2017).
  23. Hwang, J. et al. Perovskites in catalysis and electrocatalysis. *Science* **358**, 751–756 (2017).
  24. Pearce, P. E. et al. Evidence for anionic redox activity in a tridimensional-ordered Li-rich positive electrode beta-Li $_2$ IrO $_3$ . *Nat. Mater.* **16**, 580–586 (2017).
  25. Assat, G. & Tarascon, J.-M. Fundamental understanding and practical challenges of anionic redox activity in Li-ion batteries. *Nat. Energy* **3**, 373–386 (2018).
  26. McCalla, E. et al. Understanding the roles of anionic redox and oxygen release during electrochemical cycling of lithium-rich layered Li $_4$ FeSbO $_6$ . *J. Am. Chem. Soc.* **137**, 4804–4814 (2015).
  27. Zhang, T. et al. Electrospun  $\text{YMn}_2\text{O}_5$  nanofibers: A highly catalytic activity for NO oxidation. *Appl. Catal. B* **247**, 133–141 (2019).
  28. Thampy, S. et al. Role of surface oxygen vacancies in intermediate formation on mullite-type oxides upon NO adsorption. *J. Phys. Chem. C* **124**, 15913–15919 (2020).
  29. Zhang, T. et al. Promotion of low-temperature oxidation of propane through introduction of Ce into mullite oxide  $\text{YMn}_2\text{O}_5$ . *Chem-PlusChem* **87**, e202100455 (2022).
  30. Thampy, S. et al. Superior low-temperature NO catalytic performance of  $\text{PrMn}_2\text{O}_5$  over  $\text{SmMn}_2\text{O}_5$  mullite-type catalysts. *Catal. Sci. Technol.* **9**, 2758–2766 (2019).
  31. Thampy, S., Ashburn, N., Cho, K. & Hsu, J. W. P. Earth-abundant transition metal-based mullite-type oxide catalysts for heterogeneous oxidation reactions. *Adv. Energy Sustain. Res.* **2**, 2000075 (2021).
  32. Chen, Z., Liu, X., Cho, K., Chen, R. & Shan, B. Density functional theory study of the oxygen chemistry and NO oxidation mechanism on low-index surfaces of  $\text{SmMn}_2\text{O}_5$  mullite. *ACS Catal.* **5**, 4913–4926 (2015).
  33. Yang, J. et al. Origin of the superior activity of surface doped  $\text{SmMn}_2\text{O}_5$  mullites for NO oxidation: a first-principles based microkinetic study. *J. Catal.* **359**, 122–129 (2018).
  34. Hwang, J. et al. Regulating oxygen activity of perovskites to promote NO $_x$  oxidation and reduction kinetics. *Nat. Catal.* **4**, 663–673 (2021).
  35. Zhu, Y. et al. Fundamental mechanistic insights into the catalytic reactions of Li-S redox by Co single-atom electrocatalysts via operando methods. *Sci. Adv.* **9**, eadi5108 (2023).
  36. Qiao, R., Chin, T., Harris, S. J., Yan, S. & Yang, W. Spectroscopic fingerprints of valence and spin states in manganese oxides and fluorides. *Curr. Appl. Phys.* **13**, 544–548 (2013).
  37. Long, X. et al. Direct spectroscopy for probing the critical role of partial covalency in oxygen reduction reaction for cobalt-manganese spinel oxides. *Nanomaterials* **9**, 577 (2019).
  38. Wang, X. et al. Manipulating surface termination of perovskite manganate for oxygen activation. *Adv. Funct. Mater.* **31**, 2006439 (2021).
  39. Li, L., Shen, Q., Cheng, J. & Hao, Z. Catalytic oxidation of NO over TiO $_2$  supported platinum clusters I. Preparation, characterization and catalytic properties. *Appl. Catal. B* **93**, 259–266 (2010).
  40. Li, L., Qu, L., Cheng, J., Li, J. & Hao, Z. Oxidation of nitric oxide to nitrogen dioxide over Ru catalysts. *Appl. Catal. B* **88**, 224–231 (2009).
  41. Auvray, X. & Olsson, L. Stability and activity of Pd-, Pt- and Pd-Pt catalysts supported on alumina for NO oxidation. *Appl. Catal. B* **168**, 342–352 (2015).
  42. Adjimi, S. et al. Highly efficient and stable Ru/K-OMS-2 catalyst for NO oxidation. *Appl. Catal. B* **219**, 459–466 (2017).
  43. Jeong, H. et al. Controlling the oxidation state of Pt single atoms for maximizing catalytic activity. *Angew. Chem. Int. Ed.* **59**, 20691–20696 (2020).
  44. Liu, S., Wu, X., Weng, D., Li, M. & Lee, H.-R. Combined promoting effects of platinum and MnO $_x$ -CeO $_2$  supported on alumina on NO $_x$ -assisted soot oxidation: thermal stability and sulfur resistance. *Chem. Eng. J.* **203**, 25–35 (2012).
  45. Ogel, E. et al. Impact of preparation method and hydrothermal aging on particle size distribution of Pt/ $\gamma$ -Al $_2$ O $_3$  and its performance in CO and NO. *Oxid. J. Phys. Chem. C* **123**, 5433–5446 (2019).
  46. Wen, Y., Zhang, C., He, H., Yu, Y. & Teraoka, Y. Catalytic oxidation of nitrogen monoxide over La $_{1-x}$ Ce $_x$ CoO $_3$  perovskites. *Catal. Today* **126**, 400–405 (2007).
  47. Thampy, S. et al. Superior catalytic performance of Mn-mullite over Mn-perovskite for NO oxidation. *Catal. Today* **310**, 195–201 (2018).
  48. Datype, A. & Votsmeier, M. Opportunities and challenges in the development of advanced materials for emission control catalysts. *Nat. Mater.* **20**, 1049–1059 (2021).
  49. Mueller, D. N. Data collection strategies, analysis, and interpretation in AP-XAS. in *Ambient Pressure Spectroscopy in Complex Chemical Environments*, 315–331 (American Chemical Society, 2021).
  50. Zhang, H. et al. Ambient pressure mapping of resonant Auger spectroscopy at BLO2B01 at the Shanghai Synchrotron Radiation Facility. *Rev. Sci. Instrum.* **91**, 123108 (2020).
  51. Huang, Y., Pellegrinelli, C. & Wachsman, E. D. Direct observation of oxygen dissociation on non-stoichiometric metal oxide catalysts. *Angew. Chem. Int. Ed.* **55**, 15268–15271 (2016).
  52. Huang, Y., Pellegrinelli, C. & Wachsman, E. D. Reaction kinetics of gas-solid exchange using gas phase isotopic oxygen exchange. *ACS Catal.* **6**, 6025–6032 (2016).
  53. Lu, Y. et al. Identification of the active complex for CO oxidation over single-atom Ir-on-MgAl $_2$ O $_4$  catalysts. *Nat. Catal.* **2**, 149–156 (2018).

## Acknowledgements

Y.P. thanks National Natural Science Foundation of China (T2341002 and 22276104) for support. S.F. acknowledges the National Natural Science Foundation of China (21831003). Y.A.W. acknowledges the Natural Science and Engineering Research Council (NSERC) of Canada (RGPIN-2020-05903 and GECR-2020-00476). C.R. thanks the University of Hull for support. The authors thank beamline BLO2B of the Shanghai Synchrotron Radiation Facility supported by National Natural Science Foundation of China under contract No. 11227902. The authors thank the beamline BL14W1 of SSRF for providing beamtime. The authors thank

NSRL beamlines MCD-A and MCD-B (Soochow Beamline for Energy Materials) in NSRL for providing beamtime.

## Author contributions

All authors contributed to the discussion and approved the manuscript. These authors contributed equally to this work: X.W. and Q.Y. Methodology: X.W., Q.Y., Y.P. Investigation and synthesis: X.W., Q.Y. Characterizations: X.W., Q.Y., X.L., C.G., Z.L., H.Z., S.S., X.C. Supervision: X.W., Y.P. Writing—original draft: X.W., Q.Y., Y.P. Writing—review & editing: X.W., Y.W., Y.M., C.R., Y.P., J.L., S.F.

## Competing interests

The authors declare no competing interests.

## Additional information

**Supplementary information** The online version contains supplementary material available at <https://doi.org/10.1038/s41467-024-51473-9>.

**Correspondence** and requests for materials should be addressed to Yue Peng.

**Peer review information** *Nature Communications* thanks Rong Chen and the other, anonymous, reviewers for their contribution to the peer review of this work. A peer review file is available.

**Reprints and permissions information** is available at <http://www.nature.com/reprints>

**Publisher's note** Springer Nature remains neutral with regard to jurisdictional claims in published maps and institutional affiliations.

**Open Access** This article is licensed under a Creative Commons Attribution-NonCommercial-NoDerivatives 4.0 International License, which permits any non-commercial use, sharing, distribution and reproduction in any medium or format, as long as you give appropriate credit to the original author(s) and the source, provide a link to the Creative Commons licence, and indicate if you modified the licensed material. You do not have permission under this licence to share adapted material derived from this article or parts of it. The images or other third party material in this article are included in the article's Creative Commons licence, unless indicated otherwise in a credit line to the material. If material is not included in the article's Creative Commons licence and your intended use is not permitted by statutory regulation or exceeds the permitted use, you will need to obtain permission directly from the copyright holder. To view a copy of this licence, visit <http://creativecommons.org/licenses/by-nc-nd/4.0/>.

© The Author(s) 2024